

**Exercise 23**

A second order quasi-instantaneous reaction  $A_1 + A_2 \rightarrow P$  is carried out in a microreactor. Multi-point injection of reactant  $A_2$  is required to reduce the hot spot.

**Data**

Mean heat capacity of reaction mixture  $c_p = 1700 \text{ J kg}^{-1} \text{ K}^{-1}$

Density of reaction mixture  $\rho = 1142 \text{ kg m}^{-3}$

Reaction enthalpy  $\Delta H_r = -120 \text{ kJ mol}^{-1}$

Inlet concentrations  $c_{1,0} = c_{2,0} = 1.56 \text{ kmol m}^{-3}$

Total inlet flowrates  $\dot{V}_{10} = \dot{V}_{20} = 0.9 \cdot 10^{-7} \text{ m}^3 \text{ s}^{-1}$

Number of injection points for reactant  $A_2 = 6$

Equal flow partition of reactant  $A_2$

Microchannel diameter  $d = 150 \cdot 10^{-6} \text{ m}$

Overall volumetric heat transfer coefficient :  $U_v = 5 \cdot 10^6 \text{ W m}^{-3} \text{ K}^{-1}$

Cooling temperature and inlet flow temperatures  $T_c = T_{inj} = T_0 = 50^\circ \text{C}$

**Questions**

- Calculate the adiabatic temperature rise at each injection point assuming  $t_{rx} \ll t_{heat}$  and  $t_{rx} \ll t_{mx}$
- For each segment, calculate the length required to remove 50% of the reaction heat.

**Solution**

For  $j = 1$  to 6:

$$\Delta T_{ad,j} = \frac{(\dot{n}_{2,0}/N)(-\Delta H_r)}{(\rho \dot{V}_j) c_p}$$

Where  $\dot{n}_{2,0} = \dot{V}_{20} \cdot c_{2,0}$

And  $\dot{V}_j = \dot{V}_{1,0} + j \frac{\dot{V}_{2,0}}{N}$

$$T_{in,1} = T_0 + \Delta T_{ad,1}$$

$$T_{in,j} = \frac{\dot{V}_{j-1}}{\dot{V}_j} T_{out,j-1} + \frac{\dot{V}_{2,0}/N}{\dot{V}_j} T_0 + \Delta T_{ad,j}$$

Where  $T_{out,j-1}(50\% \text{ heat removal}) = T_c + 0.5(T_{in,j-1} - T_c)$

$$L_j = u_j \frac{\rho c_p}{U_V} \ln \left( \frac{T_{in,j} - T_c}{T_{out,j} - T_c} \right)$$

With  $u_j = \frac{\dot{V}_j}{\pi \frac{d^2}{4}}$

j	$\dot{V}_j$ (m <sup>3</sup> /s)	$u_j$ (m/s)	$\Delta T_{adj}$ (K)	$T_{in,1}$ (°C)	$T_{out,1}(50\%)$ (°C)	$\tau_j$ (s)	$L_j$ (m)
1	$1.05 \cdot 10^{-7}$	5.9	13.8	63.8	56.9	0.27	1.6
2	$1.20 \cdot 10^{-7}$	6.8	12.1	68.1	59.0	0.27	1.8
3	$1.35 \cdot 10^{-7}$	7.6	10.7	68.7	59.4	0.27	2.1
4	$1.50 \cdot 10^{-7}$	8.5	9.6	68.1	59.0	0.27	2.3
5	$1.65 \cdot 10^{-7}$	9.3	8.8	67.0	58.5	0.27	2.5
6	$1.80 \cdot 10^{-7}$	10.2	8.0	65.8	57.9	0.27	2.7

**13.0**